IN THE CLAIMS:

Please cancel claims 1 to 22 without prejudice, and please replace by inserting new claims 23 to 43 to as follows:

23. A process for producing monolithic supported catalysts for gas-phase oxidation comprising

coating a catalyst support with a suspension,

wherein the suspension comprises catalytically active composition comprising at least one type of TiO_2 and 1-10% by weight of at least one surfactant of the formula

$$R_nY_mX$$

where R is a hydrophobic group of the surfactant and n is 1, 2 or 3; Y is a hydrophilic group of the surfactant and m is 0, 1, 2 or 3, and X is a hydrophilic head group of the surfactant; and the percent by weight is based upon the total weight of the composition.

24. The process as claimed in claim 23,

wherein the surfactant comprises from 2 to 5% by weight based upon the total weight.

25. The process as claimed in claim 23,

wherein the head group X present in the surfactant is a functional group selected from the group consisting of

carboxylate, polycarboxylate, phosphate, phosphonate, sulfate and sulfonate.

26. The process as claimed in claim 25,

wherein at least one of the functional groups of the head group X is selected from the group consisting of free acid group, ammonium salt, and alkaline earth metal salt.

27. The process as claimed in claim 23,

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wherein the hydrophilic group Y is bound to a central atom of the head group X either directly or via an oxygen.

28. The process as claimed in claim 23,

wherein the hydrophobic group R of the surfactant used is bound to the head group X via a hydrophilic group Y.

29. The process as claimed in claim 23,

wherein hydrophobic groups R of the surfactant used are selected from the group consisting of saturated alkyl radicals with carbon building blocks having from 5 to 30 carbon atoms, unsaturated alkyl radicals with carbon building blocks having from 5 to 30 carbon atoms; and

branched alkyl radicals with carbon building blocks having from 5 to 30 carbon atoms and are bound either directly or

via aryl groups to a group selected from the group consisting of the hydrophilic group Y and the head group X.

30. The process as claimed in claim 23,

wherein the hydrophilic group Y of the surfactants used comprises polymeric alkoxy units whose degree of polymerization is from 1 to 50 monomer units.

31. The process as claimed in claim 23,

wherein said at least one surfactant is selected from the group consisting of calcium alkylarylsulfonate, alkylphenol ethoxylate, ammonium alkylarylsulfonate, calcium dodecylbenzenesulfonate, polyethoxy (dinonyl phenyl ether phosphate), polyoxoethylene (lauryl ether phosphate), polyethoxy (tridecyl ether phosphate), calcium dodecylbenzenesulfonate, tridecyl phosphate ester, ethoxylated phosphated alcohol, alkyl polyoxyethylene ether phosphate, and ammonium nonyl phenyl ether sulfate.

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32. The process as claimed in claim 23,

wherein the catalytically active composition further comprises V_2O_5 as an additional component.

33. The process as claimed in claim 23,

wherein the catalytically active composition comprises promoters.

34. The process as claimed in claim 23,

wherein the catalyst support used is at least one material selected from the group consisting of cordierite, silicate, silicon dioxide, silicon carbide, aluminum oxide, aluminate, metal and metal alloy.

35. The process as claimed in claim 23,

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wherein a catalyst support body used is selected from the group consisting of a honeycomb, a support having open cross-channel structure, a support having closed cross channel structure, and mixtures thereof.

36. The process as claimed in claim 35, wherein

wherein the catalyst support body used is a honeycomb having a cell density of a number of channels, of from 100 to 400 csi (cells per square inch).

37. A method for preparing phthalic anhydride comprising

a gas-phase oxidation reaction of o-xylene by contacting said o-xylene with a monolithic supported catalyst obtainable by the process as claimed in claim 23 in an adiabatic reactor in combination with an isothermally operated reactor.

38. A method for preparing phthalic anhydride comprising a gas-phase oxidation reaction of naphthalene by contacting said naphthalene with a monolithic supported catalyst obtainable by the process as claimed in claim 23 in an adiabatic reactor in combination with an isothermally operated reactor.

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39. A method for preparing phthalic anhydride comprising a gas-phase oxidation reaction of a mixture of o-xylene and naphthalene by contacting said mixture of o-xylene and naphthalene with a monolithic supported catalyst obtainable by the process as claimed in claim 23 in an adiabatic reactor in combination with an isothermally operated reactor.

40. The method as claimed in claim 37, wherein the adiabatic reactor has upstream gas cooling in combination with an isothermally operated reactor.

41. The method as claimed in claim 37, wherein the adiabatic reactor has upstream gas cooling, where gas cooling and the reaction are carried out in a joint apparatus, in combination with an isothermally operated reactor.

42. The method as claimed in claim 37,

wherein the adiabatic reactor has upstream gas cooling and downstream gas cooling, where gas cooling and the reaction are carried out in a joint apparatus, in combination with an isothermally operated reactor.

43. A catalyst comprising

a catalyst support coated with a suspension; and said suspension comprises a catalytically active composition comprising

at least one type of TiO_2 and 1-10% by weight of at least one surfactant of the formula

$$R_nY_mX$$

where R is a hydrophobic group of the surfactant and n is 1, 2 or 3; Y is a hydrophilic group of the surfactant and m is 0, 1, 2 or 3, and X is a hydrophilic head group of the surfactant; and

the percent by weight is based upon the total composition weight.

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